

## Wave Breaking and Turbulence Model of Spume Droplet Production

Following Andreas, we can represent the rate of TKE converted to potential energy in the surface tension of droplets as

$$d(\Delta F) / dt = \Sigma \int 4 / 3 \pi r^2 n_s(r) dr$$

where  $\Delta F$  is some fraction of  $P$  the total energy input to breaking waves ( $\text{W/m}^2$ )

$\Sigma$  the surface tension of the water-air interface ( $\text{Nt/m}$ )

$r$  the droplet radius

$n_s(r)$  the number of droplets produces per second per square meter of surface.

$P$  is actually an integral over the wavenumber space of wave energy transfer spectrum. Before looking at  $P$ , consider the common representation of the dissipation of **turbulent** kinetic energy,  $\epsilon$ ,

$$\epsilon = 2\nu \int k^2 E(k) dk$$

where  $\nu$  is the kinematic viscosity and  $E(k)$  the energy spectral density.

## Energy Cascade

At any given wavenumber energy transfers from larger to smaller scales are characterized by the spectral transfer parameter,  $T(k)$ . In the inertial subrange,  $T(k)=\epsilon$ ; for wavenumbers exceeding the Kolmogorov wavenumber,  $k_\eta$ ,  $T(k)$  decreases. In the inertial subrange, the energy spectrum is given by

$$E(k) = \alpha \epsilon^{2/3} k^{-5/3}$$

The transfer of energy in the spectral domain is described by the equation

$$\frac{\partial E}{\partial t} = -\frac{\partial T}{\partial k} - \nu k^2 E$$

Tennekes and Lumley (1972) give a form of  $T(k)$  that is consistent with this budget equation and the -5/3 subrange behavior

$$E(k) = \alpha \epsilon^{2/3} k^{-5/3} \exp\left[-\frac{3}{2} \alpha (k\eta)^{4/3}\right]$$

$$T(k) = \epsilon \exp\left[-\frac{9}{4} \alpha (k\eta)^{4/3}\right]$$

where  $\eta=(\nu^3/\epsilon)^{1/4}$  is the Kolmogorov microscale.

## Application to Droplets

Since we are interested in droplets of some size, we want  $T(r)$  instead of  $T(k)$ . It is simple to show that in the inertial subrange,  $E(r)$  is given by

$$E(r) = \frac{\alpha}{\pi^{2/3}} \varepsilon^{2/3} r^{-1/3}$$

$$T(r) = \varepsilon \exp\left[-\frac{9}{4} \alpha \left(\frac{\pi \eta}{r}\right)^{4/3}\right]$$

Now, we relate energy input per unit area versus unit volume following Newell and Zakharov; the Kolmogorov scale at the air-sea interface is given by

$$\eta = \frac{\nu}{P^{1/3}}$$

or  $P = \varepsilon \eta$ . Thus, by analogy we can write  $T_p(r)$  as

$$T_p(r) = P \exp\left[-\frac{9}{4} \alpha \left(\frac{\pi \eta}{r}\right)^{4/3}\right]$$

## Partitioning of Energy

In the absence of droplet processes,  $T_p(r) \approx P$  for large  $r$ ; therefore,  $\partial T/\partial r$  is essentially 0. This is the definition of the inertial subrange; i.e., energy isn't lost at these scales but transferred to smaller scales where it is eventually dissipated.

Suppose we now assume that some *small* fraction of the energy being transferred in  $r$ -space is lost to the droplets. This implies

$$\frac{4\pi}{3} \sigma r^2 n_s(r) = -\frac{\partial T}{\partial r} = \frac{f}{l} T(r)$$

where  $f$  is an unknown constant,  $\sigma = \Sigma/\rho_w = 7.4 \times 10^{-5} \text{ m}^3/\text{s}^2$ , and  $l$  an 'appropriate' size scale. This gives a final expression for  $n_s$  is

$$\frac{4\pi r^3}{3} n_s(r) = \frac{f \text{ Pr}}{\sigma l} \exp\left[-\frac{9}{4} \alpha \left(\frac{\pi \eta}{r}\right)^{4/3}\right]$$

It is not obvious to me what should be used for  $l$ . Possibilities include  $\eta$ ,  $(rE(r))^{1/2}$ , some local wave scale, or something associated with surface tension.

## Escaping the Interface

This approach gives us some estimate of the droplet spectrum produced by the breakdown of the air-water interface, but it says little about the introduction of those droplets into the turbulent surface layer over the water. To do this, we postulate that droplets will spend a significant time airborne if their fall velocity is less than the local wind speed times the local slope of the waves. If we assume a Gaussian distribution of horizontal wind speed fluctuations, then an error function describes the integral probability that a droplet of size  $r$  is ejected from the top of the wave. Thus

$$\frac{4\pi r^3}{3} n_s(r) = \frac{f Pr}{\sigma l} \exp\left[-\frac{9}{4} \alpha \left(\frac{\pi \eta}{r}\right)^{4/3}\right] * \left[1 + \operatorname{erf}\left(\frac{U(h) - V_f / \text{Slope}}{\sigma_u}\right)\right] / 2$$

where  $V_f(r)$  is the gravitational settling speed of the droplet,  $U(h)$  the mean wind speed at height  $h$ , and  $\sigma_u$  the standard deviation of wind speed fluctuations at  $h$ . For large droplets, low wind speeds, or small wave slopes  $\operatorname{erf} \rightarrow -1$  and no droplets are observed. For very small droplets,  $\eta/r$  becomes large, and no droplets are produced.

$P$  energy wave breaking ( $\text{W/m}^2$ )

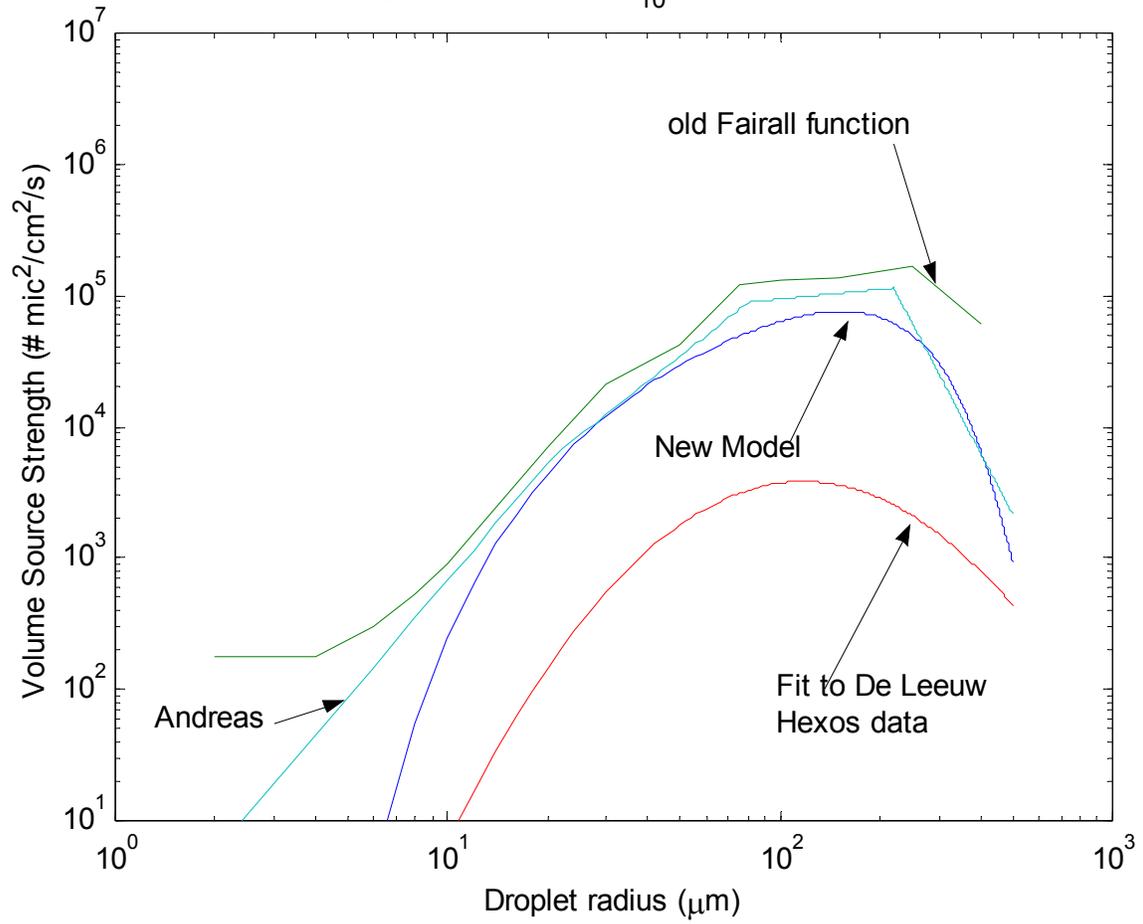
$\sigma$  surface tension

$r$  droplet radius

$\eta$  Kolmogorov microscale =  $\nu/P^{1/3}$

$f$  fraction of  $P$  going into droplet production

Source strength from deLeeuw  $u_{10}=21$  m/s,  $h=4.0$  m  $z=11$  m



## Background

The conservation equation for the ensemble mean of variable  $x$ , denoted as  $X$ , is

$$\frac{\partial X}{\partial t} + \nabla_h X \cdot \mathbf{u}_h = -\frac{\partial(\overline{w'x'})}{\partial z} + \overline{S_x}$$

where the subscript  $h$  denote horizontal components and  $S_x$  represents the source terms for the variable  $x$ . The quantity of interest is the Reynolds flux enclosed in the parentheses.

$$\text{Stress: } \vec{\tau} = \rho \{ \langle w'u' \rangle \vec{i}_x + \langle w'v' \rangle \vec{i}_y \}$$

$$\text{Sensible heat: } H_s = \rho c_p \langle w'T' \rangle$$

$$\text{Latent heat: } H_l = \rho L_e \langle w'q' \rangle$$

Bulk Formula for **Surface** fluxes :

$$\tau = -\rho C_d U[u]$$

$$H_s = \rho c_p C_h U[T_o - \theta]$$

$$H_l = \rho L_e C_E U[q_o - q]$$

U=wind speed    T=temperature    q=specific humidity

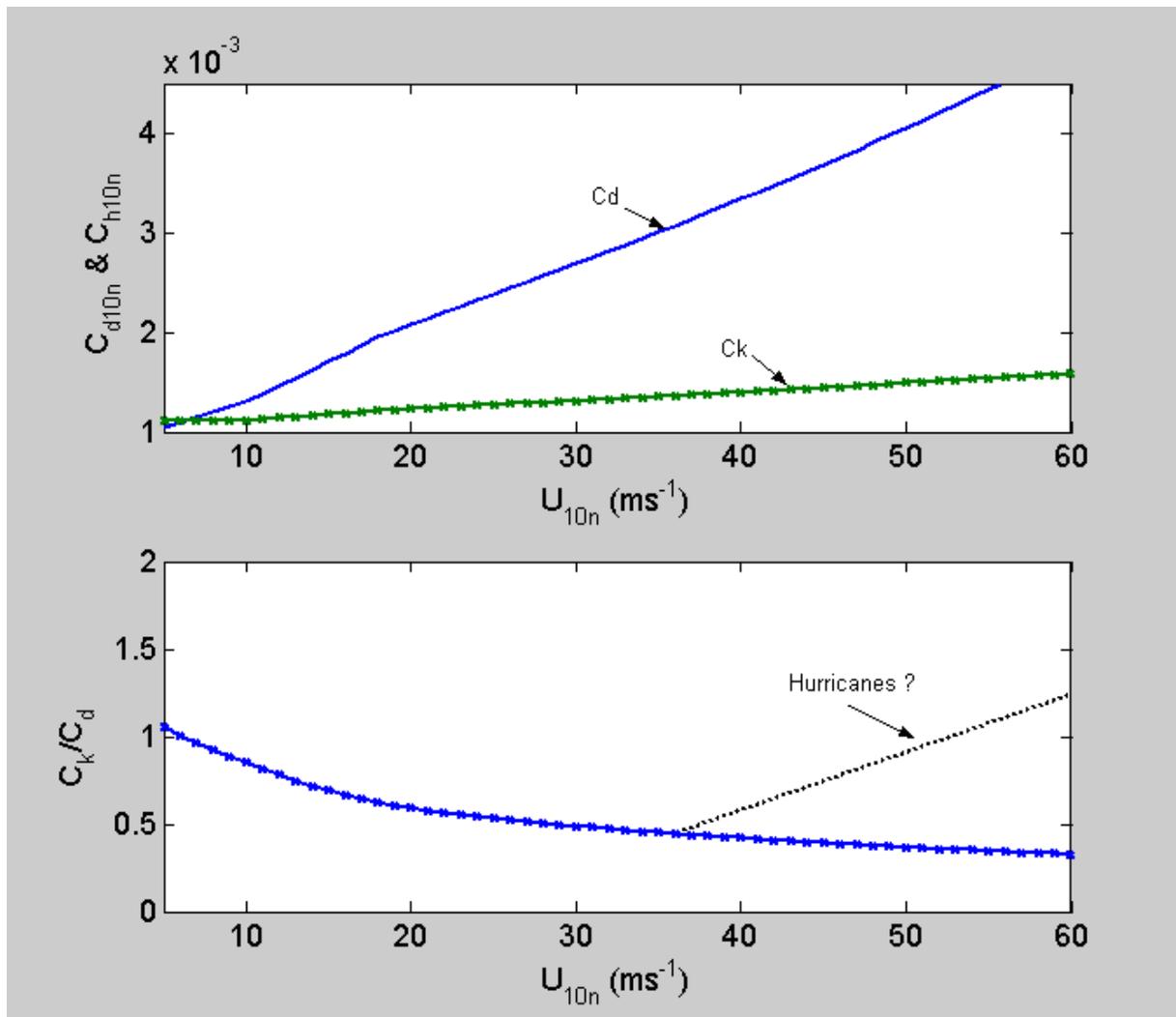
$C_h = C_E \approx 1.15 \times 10^{-3}$      $C_d \approx$  Increases with wind speed

## Sea Spray and Hurricanes

Enthalpy flux = Sensible + Latent heat fluxes

$$H_k = H_s + H_l \quad \text{therefore } C_k = C_h + C_e$$

Emanuel (1995) showed relationship between ratio of  $C_k/C_d$  affected the maximum strength of hurricanes. A ratio of 1.5 was required to get a hurricane with 80 m/s wind speed.



## Questions:

Does sea spray significantly affect hurricane dynamics?  
What is required to parameterize sea spray effects?

## Sidebar:

Note evaporation of droplets changes partition of Hs and HI,  
but does not change Hk!!

## Steps in the process:

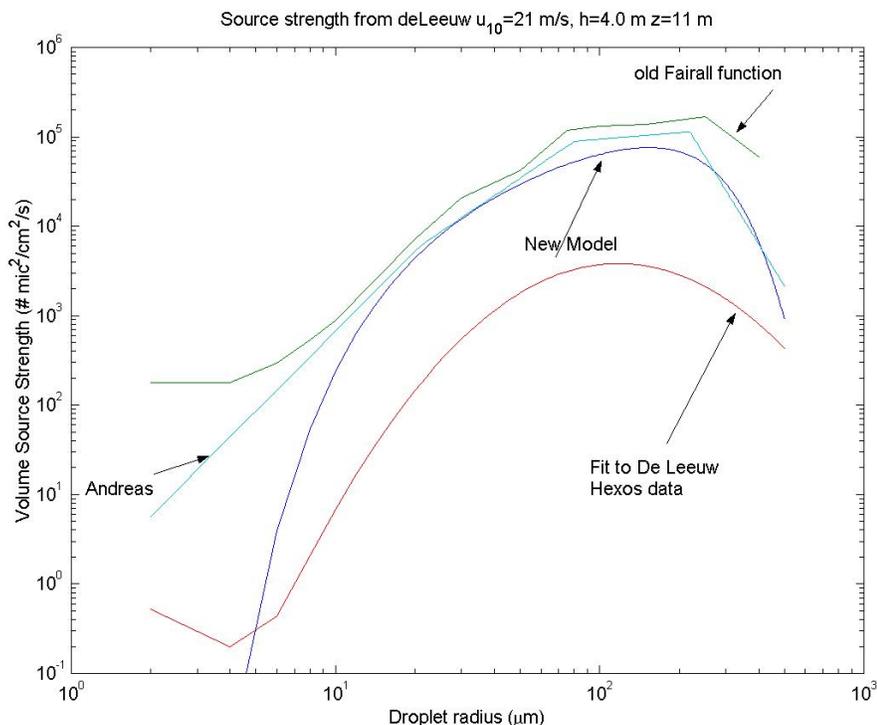
Characterize the surface source strength,  $s_n$ , of the ocean.  
Characterize the thermodynamics of droplet heat/moisture transfer.

Develop parameterization.

See effect on hurricanes.

## Definition

$s_n = \# \text{drops of radius } r / (\text{ocean surface area } s \text{ dr})$   
volume source =  $4/3\pi r^3 s_n$



## Single Droplet View

Ocean temperature,  $T_s$

Air temperature,  $T_a$

Droplet of radius  $r_o$  is ejected as seawater at  $T=T_s$ , it cools to the wet bulb temperature,  $T_w$ , it evaporates at some rate,  $E$ . After some time,  $t$ , it re-impacts the sea surface at size  $r_f$ .

Net heating of the air by direct transfer from the ocean

$$Q_{si} = \rho_w c_{pw} \frac{4}{3} \pi r_o^3 (T_s - T_w)$$

Net evaporation of sea spray droplet

$$Q_{li} = \rho_w L_e \frac{4}{3} \pi (r_o^3 - r_f^3)$$

To define the impact of a spectrum of droplets, integrate over  $s_n$

$$Q_s = \rho_w c_{pw} \left[ \int \frac{4}{3} \pi r_o^3 s_n(r_o) dr_o \right] (T_s - T_w)$$

$$Q_l = \rho_w L_e \left[ \int \frac{4}{3} \pi r_o^3 s_n(r_o) \left( 1 - \left( \frac{r_f}{r_o} \right)^3 \right) dr_o \right]$$

## Single Droplet Thermodynamics

Mass lost to evaporation

$$\dot{M} = -4\pi D_v f_p r \rho_a [q_s(T_r) - q_a] = 4\pi r^2 \dot{r}$$

Cooling by evaporation

$$E = -L_e \dot{M} = 4\pi D_v f_p r \rho_a L_e [q_s(T_r) - q_a]$$

Heating by direct heat transfer from drop to air

$$H = 4\pi D_T f_p r \rho_a c_{pa} [T_r - T_a]$$

Wet bulb temperature defined by H=E

$$D_T c_p [T_w - T_a] = D_v L_e [q_s(T_w) - q_a]$$

Solve by expanding Clausius-Claperyon relation

$$T_a - T_w = \frac{(1 - \beta)}{\gamma} (1 - S)$$

$$\frac{\partial q_s}{\partial T} = \gamma q_s; \beta = \left(1 + \frac{L_e}{c_p} \gamma q_s\right)^{-1}$$

Time constants

$$\tau_r = r / \dot{r}; \tau_l = M / \dot{M} = 3\tau_r; \tau_s = c_{pw} M / H$$

$$\tau_f = h / V_f$$

## Modeling Approaches

### Explicit Droplet Models

- \*PBL turbulence model (k-theory, LES, DNS, waves)
- \*Throw in droplets according to  $s_n$
- \*Account for droplet fall velocity/turbulent transport
- \*Compute evaporation as function of size
- \*Account for loss at surface
- \*Can use Lagrangian or Eulerian approaches

Edson et al., 1994: K-theory turbulence with Lagrangian droplets

Keprt/Fairall (1999): 1.5-order closure BL , 10-bin salt spectra

### Scaling Models

- \*Inject droplets at a specified (parameterized) source height
- \*Ignore turbulence, assume lifetime dominated by fall velocity
- \*Calculate thermodynamic effects based on balance of time constants as a function of droplet size.
- \*Produce parameterization  $Q_s$ ,  $Q_l$  as function of  $U$

Andreas (1992, 1999)

Fairall et al. (1994)

### Empirical Models

- \*Get data on droplet concentrations
- \*Convert to source function
- \*Do a fit, extrapolate to higher wind speeds

## Feedback Parameterization

Start with no-feedback calculations  $H_{so}$ ,  $H_{lo}$ ,  $Q_{so}$ ,  $Q_{lo}$   
Droplet evaporation cools profile by  $\delta T_a$  and moistens by  $\delta T_d$

$$H_s = \rho c_p C_h U [T_s - T_a - \delta T_a]$$

$$H_l = \rho c_p L_e U [q_s(T_s) - q_s(T_d + \delta T_d)]$$

$$Q_s = Q_{so}$$

$$Q_l = Q_l(T_a - \delta T_a, T_d + \delta T_d) = \alpha Q_{lo}$$

Feedback coefficient defined by assuming evaporation is limited by the sources of heat available

$$feed = \frac{Q_{lo}}{Q_{lo} + H_s + Q_s + H_\epsilon}$$

$$\delta T_a = feed * (T_a - T_w)$$

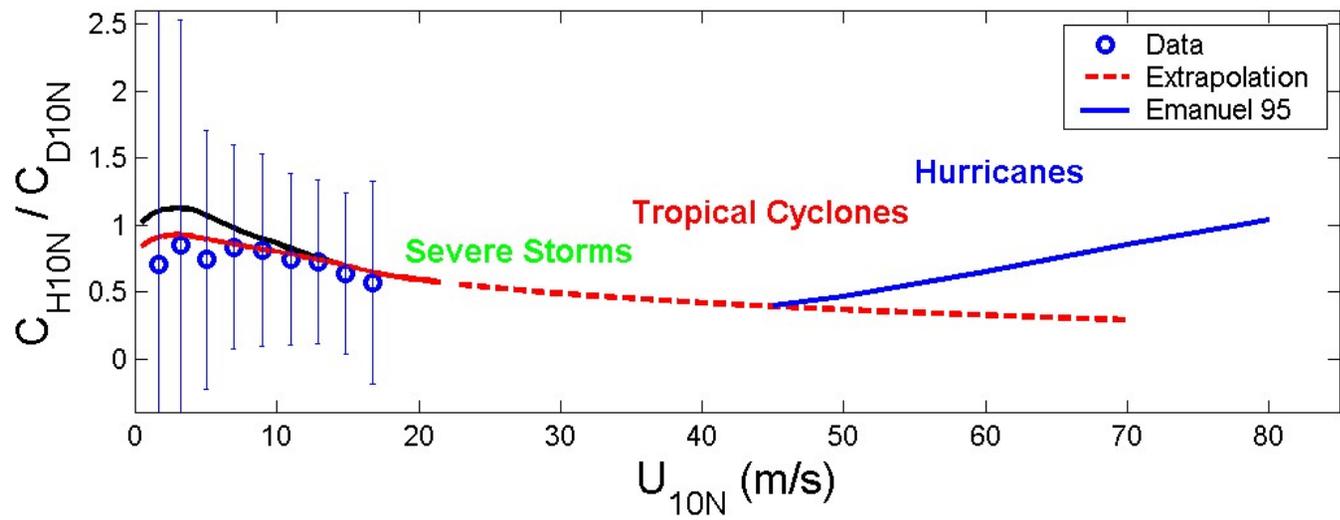
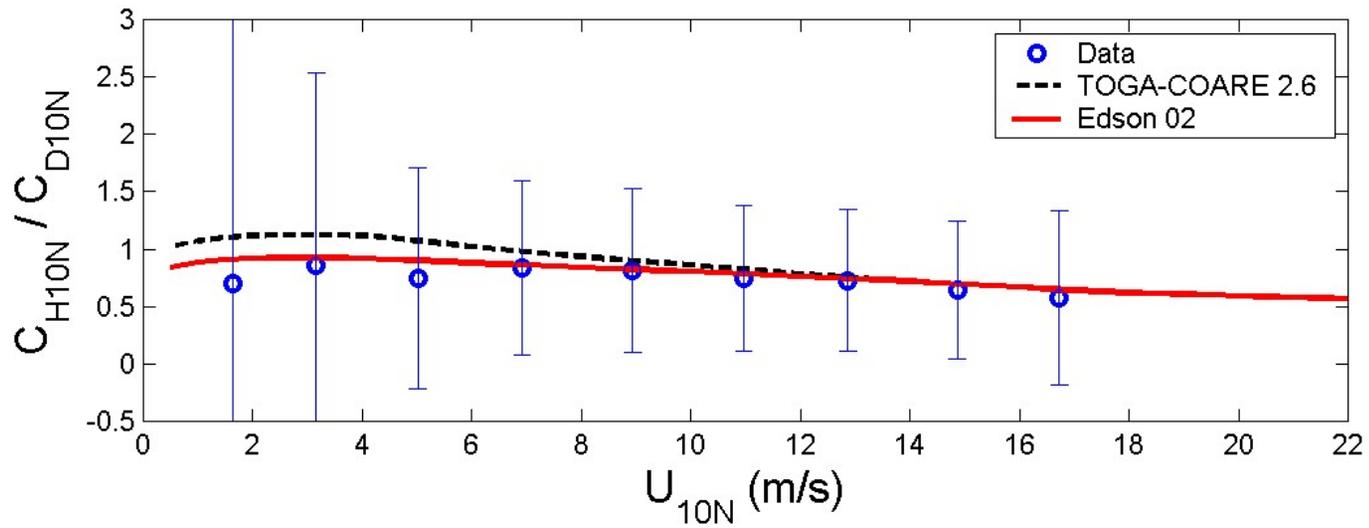
$$\delta T_d = \frac{\beta}{1 - \beta} \delta T_a$$

## Energy Fluxes With Droplet Evaporation

$$\text{Total sensible heat} = H_s + Q_s - Q_l = H_s + Q_s - \alpha Q_{l0}$$

$$\text{Total latent heat} = H_l + Q_l = H_l + \alpha Q_{l0}$$

$$\text{Total enthalpy} = H_s + H_l + Q_s$$



Thermodynamic Limits in Scaling Model (no feedback)

$$s_n(r, U) = W(U) f_n(r)$$

\*Droplet heat flux

$$Q_s = \rho_w c_{pw} \left[ \int \frac{4}{3} \pi r_o^3 s_n(r_o) dr_o \right] (T_s - T_w)$$

because  $T_s \ll T_f$ , this integral is simple

$$Q_s = \rho_w c_{pw} W(U) S_v (T_s - T_w); S_v = 5 \times 10^{-6} \text{ m / s}$$

\*Droplet evaporation flux

$$Q_l = \rho_w L_e \left[ \int \frac{4}{3} \pi r_o^3 s_n(r_o) \left(1 - \left(\frac{r_f}{r_o}\right)^3\right) dr_o \right]$$

$$r_f = r_{eq} + (r_o - r_{eq}) \exp(-\tau_f / \tau_l)$$

because  $T_l \gg T_f$ , we expand exponential

$$\left(1 - \left(\frac{r_f}{r_o}\right)^3\right) = \frac{3\tau_f}{\tau_l} \left(1 - \frac{r_{eq}}{r_o}\right)$$

$$Q_l = \rho_a L_e h(U) W(U) \beta q_s(T_a) \{4\pi D_v \int \frac{f_p r f_n(r)}{V f(r)} dr\} \left(1 - \frac{r_{eq}}{r_o}\right)$$

$$\{ \} = S_a = 0.125 \text{ s}^{-1}$$